

Calculation of equilibrium composition and temperature of n-decane (kerosene surrogate) combustion products

Background

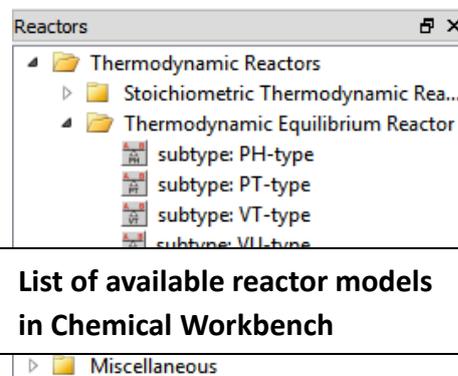
Composition and temperature of the combustion products is an integral part of the analysis of power, energy and transportation systems. It is widely used for efficiency evaluation, thermal analysis, as well as initial guess/conditions for more detailed studies of the systems under consideration.

Problem statement

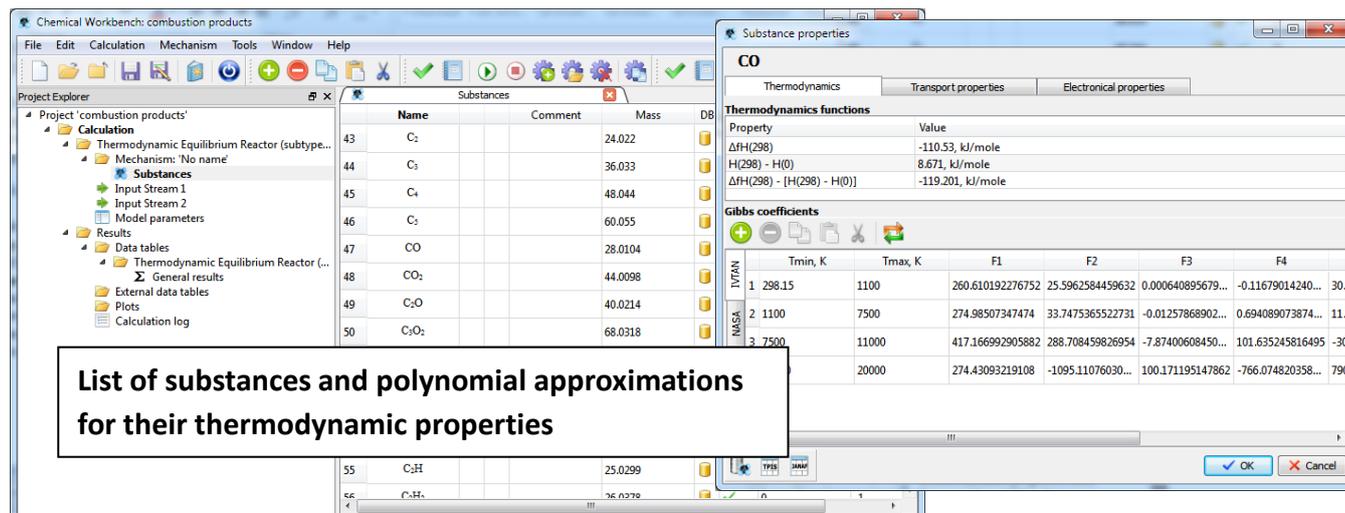
It is required to calculate equilibrium temperature and composition of the combustion products of aviation kerosene surrogate n-decane $C_{10}H_{22}$ for a range of mixture equivalence ratio. Initial temperature of kerosene-air is 600K, initial pressure 10 atm. Mixture equivalence ratio is 0.5 – 3.

Problem setup in Chemical Workbench

To calculate the equilibrium composition and temperature for n-decane-air combustion, we use the complete **chemical equilibrium model TER_PH (combustion at adiabatic conditions and constant pressure)**, available in Chemical Workbench. This model requires information only about list of all possible products, their thermodynamic properties (specific heat, enthalpy of formation, standard state entropy) and initial conditions. No guess about chemical reaction equations in the system is required



The **list of possible combustion products (mechanism)** is generated automatically by query to KintechDB database, which is tightly integrated with Chemical Workbench and provide reference thermodynamic properties data for more than 4100 substances. For n-decane combustion the query to database generates the list of 423 possible substances, composed of elements C, H, O, N, which constitute initial mixture: n-decane ($C_{10}H_{22}$) and air ($0.2 O_2 + 0.78 N_2$). Their thermodynamic properties are also loaded from database.



Name	Comment	Mass	DB
43	C ₂	24.022	
44	C ₃	36.033	
45	C ₄	48.044	
46	C ₅	60.055	
47	CO	28.0104	
48	CO ₂	44.0098	
49	C ₂ O	40.0214	
50	C ₃ O ₂	68.0318	
55	C ₂ H	25.0299	
56	C ₂ H ₂	26.0278	

Property	Value
$\Delta H(298)$	-110.53, kJ/mole
$H(298) - H(0)$	8.671, kJ/mole
$\Delta H(298) - [H(298) - H(0)]$	-119.201, kJ/mole

	Tmin, K	Tmax, K	F1	F2	F3	F4
IVTAN	1 298.15	1100	260.610192276752	25.5962584459632	0.000640895679...	-0.11679014240...
MASK	2 1100	7500	274.98507347474	33.7475365522731	-0.01257868902...	0.694089073874...
	3 7500	11000	417.166992905882	288.708459826954	-7.87400608450...	101.635245816495
		20000	274.43093219108	-1095.11076030...	100.171195147862	-766.074820358...

Initial mixture composition

Stream name	Comment
Flow Rate	1, mole/s
Temperature	600, K
Fraction units	Mole

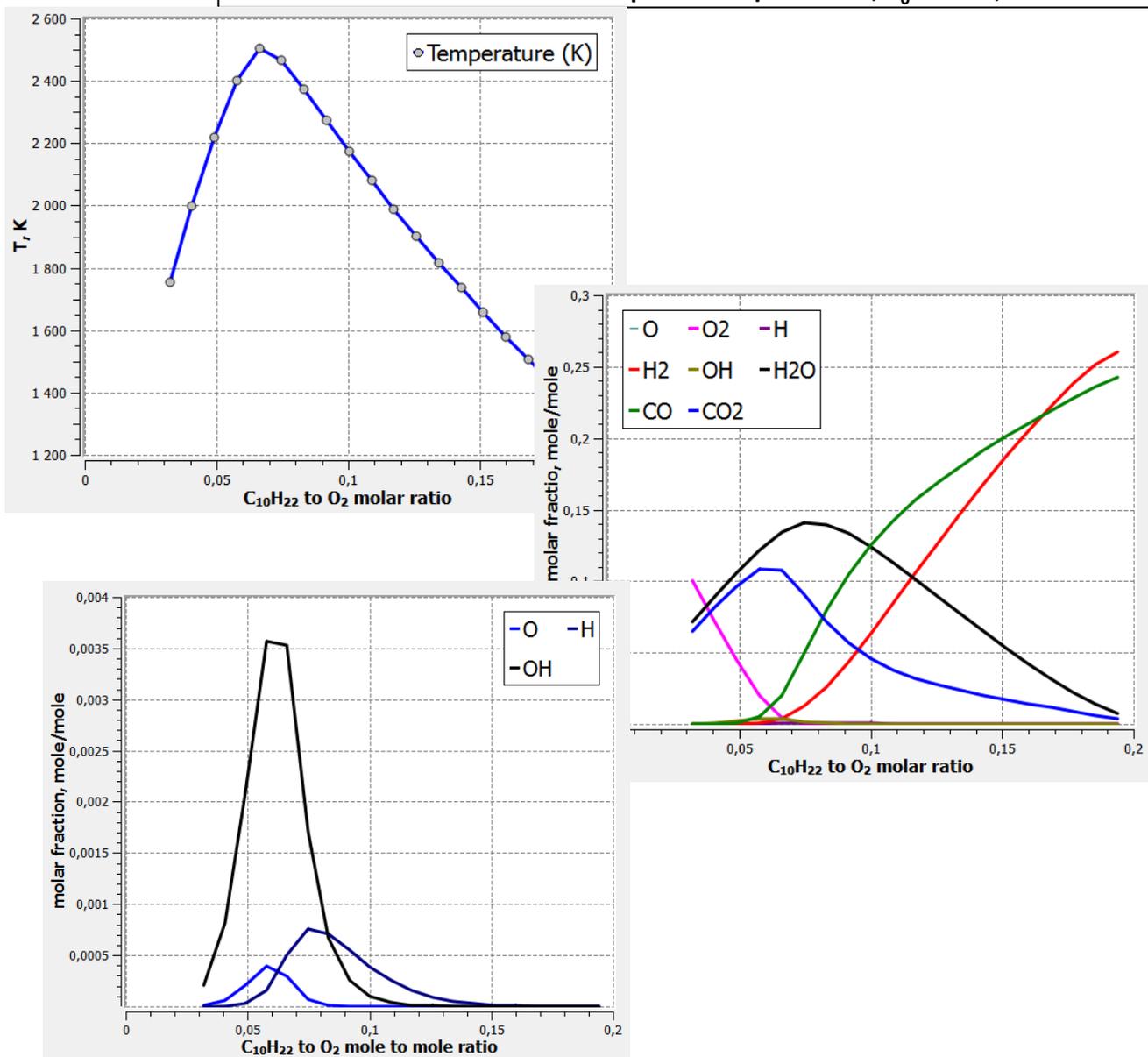
Substances fractions			
Substance	Fraction		
1	C ₁₀ H ₂₂	Variable	f_c
2	O ₂	1	f_o
3	N ₂	3.76	f_n

The **initial mixture** is set in the same input stream of the reactor with composition $x C_{10}H_{22} + O_2 + 3.76 N_2$ (in moles), where $x = 0.0322 - 0.194$ ($\varphi = 0.5 - 3$). **Initial temperature 600K, reactor pressure 10 atm.**

Results

As it would be expected, the maximum temperature of n-decane combustion is achieved at near-stoichiometric conditions. The maximum value (among) of temperature is 2502 K. At fuel-rich conditions the concentration of CO and H₂ increases, while other combustion products are absent due to lack of oxygen. The radicals concentration is low, concentration of H and O is below 0.001 molar fraction, for OH it is of order of several 0.001.

Equilibrium temperature and composition of n-decane/air combustion
products: $\phi = 0.5 - 3$, $T_0 = 600\text{K}$, $P = 10\text{ atm}$



Next steps

1. Keep only C₁₀H₂₂, O₂, N₂, CO, CO₂, H₂, N₂ in the species list and see how the combustion temperature will increase due to lack of dissociation of combustion products
2. Put fuel C₁₀H₂₂ with temperature 300K as a separate input stream of TER_PH of reactor model. Allow reactor model automatically account for different temperatures of separate streams. Thus tedious calculation of initial mixture temperature is omitted.